

Extrudate Swell of Monodisperse Polystyrenes Ben Robertson, Richard Thompson, Tom McLeish (Durham University)

Introduction

Extrudate (or die) swell happens when a polymer melt flow exits a contraction. It is a problem in industrial polymer extrusion, potentially deforming the extruded product.

The Multi-Pass Rheometer

The Multi-pass rheometer (MPR) can be used to observe polymers under flow.

V_{in}— D_{ρ}

Terms Describing the Extrudate Swell Problem The swelling ratio, $B=D_{e}/d$ describes how much the flow swells by upon leaving the extruder.

The important parameters here are the Rouse and reptation Weissenberg numbers; $W_{Rouse} = \dot{\gamma} \cdot \tau_R$ and $W_{reptation} = \dot{\gamma} \cdot \tau_d$ which increase with the flow input velocity. They describe how much the polymer chains are stretched by or oriented by the process flow. Relaxation of this chain stretch and orientation occurs at the die exit/ in the form of extrudate swell.

Moving a single piston at a controlled rate can provide extrudate swell measurements to compare to simulations. We have designed a capillary test section to perform isothermal extrusions in which observation of swelling ratios as a function of time is possible up to high shear rates. A direct comparison with *flowSolve* is now possible.





Low W_R extrudate Swell

High W_R extrudate Swell

Computer Simulations

Flow simulations were performed using the fluid dynamics package/ finite element solver *flowSolve*. The Rolie-Poly constitutive equation was used to fit the rheology of polystyrenes.

 $\frac{d\sigma}{dt} = \kappa \cdot \sigma + \sigma \cdot \kappa^{T} - \frac{1}{\tau_{d}} (\sigma - I) - \frac{2}{\tau_{r}} (\frac{\lambda - 1}{\lambda}) \sigma - \frac{2\beta}{\lambda \tau_{r}} (\frac{\lambda - 1}{\lambda}) (\sigma - I))$ Constraint Fluid flow Chain Chain Stress release Stretching orientation Simulated Extrudate Swell for 262K Polystyrene . The brighter colours indicate areas of higher stress.

Agreements

flowSolve correctly predicts the low shear 1.6extrudate swell and the 1.5of increased m 14 onset swelling in the chain stretching regime. The theory over-predicts swelling above W_R≈7 due limitations in the to apparatus.

Using a higher molecular Experimental Data 2.25 ---- flowSolve Predictions weight polymer gives a better fit further into the 2.00 stretching regime (due 1.75 to the lower shear rates required) but a poorer fit at low shear due to 1.25 polydispersity the of 1.10 -0.1 polymer. This will be corrected for in future work.



Experimental and theoretical extrudate swells for 262K polystyrene

Swelling ratios fit well to a single curve at high Rouse Weissenberg numbers despite the different molecular







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